

### **DairyNF1 Membrane Series**

# Product Description

Membrane material: PA

MWCO: 150-300D

Outer wrap: Net

**Application:** Whey desalination

**Spacer:** 31mil or 46 mil

Feature: Conform to 3A Standard

## **Membrane Characteristics**

Product	Water Flux LMH	Salt Rejection /MgSO4	Salt Rejection /NaCl
Dairy NF1	35	>98%	/

Test Condition: 2000 mg/L MgSO4,110 psi(0.76Mpa),77°F (25°C),pH 8,15% recovery.

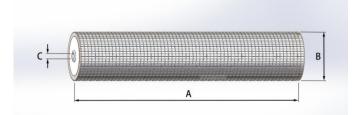
### **Product Specifications**

Model	Spacer (mil)	Membrane area (ft2/m2)	Outer wrap	
3838	31	75 (7.0)	Net	
2040	31	77 (7.2)	NI-4	
3840	46	60 (5.6)	Net	
8038	31	310 (32.5)	Net	
	46	260 (24.2)		
8040	31	310 (32.5)	NI 4	
	46	260(24.2)	Net	

## **Operating and Design Information**

Maximum Pressure Drop	70-400PSI		
Chlorine Tolerance	600PSI		
M	Operation: 50°C		
Maximum Feed Turbidity	Cleaning: 85°C		
Maximum Food SDI (15 minutes)	Continuous Operation: 3-9		
Maximum Feed SDI (15 minutes)	Chemical Cleaning: 2-10.5		
<b>Maximum Pressure Drop</b>	<15psi		
Chlorine Tolerance	500ppm/h,dechlor is recommended		
Maximum Feed Turbidity	<1NTU		
Maximum Feed SDI (15 minutes)	<5		

### **Nominal Dimensions**



Products	Dimensions-(in/mm)		
	A	В	C
Dairy NF1-3838-31-C-0830	38 (965)	3.8 (97)	0.83 (21)
Dairy NF1-3840-31/46-C-0830	38.75 (984)	3.8 (97)	0.83 (21)
Dairy NF1-8038-31/46-C-1139	38 (965)	7.9 (200)	1.125 (28.6)
Dairy NF1-8040-31-C-1125	40 (1016)	7.9 (200)	1.125 (28.6)

### DATA SHEET



### **DairyNF2 Membrane Series**

# Product Description

Membrane material: PA

**MWCO:** 150-300D

Outer wrap: Net

Application: Lactose desalination

Spacer: 31mil or 46 mil

Feature: Conform to 3A Standard

#### **Membrane Characteristics**

Product	Water Flux	Salt Rejection	Salt Rejection
	LMH	/MgSO4	/NaCl
Dairy NF2	45	>96%	/

Test Condition: 2000 mg/L MgSO4,110 psi(0.76Mpa),77°F (25°C),pH 8,15% recovery.

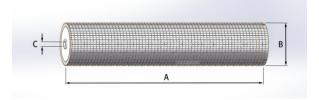
### **Product Specifications**

Model	Spacer (mil)	Membrane area (ft2/m2)	Outer wrap	
3838	31	75 (7.0)	Net	
2940	31	77 (7.2)		
3840	46	60 (5.6)	Net	
8038	31	310 (32.5)	Net	
	46	260 (24.2)		
8040	31	310 (32.5)	Net	
	46	260(24.2)		

## **Operating and Design Information**

<b>Typical Operating Pressure</b>	70-400PSI		
<b>Maximum Operating Pressure</b>	600PSI		
Marinayan Tanan aradaya	Operation: 50°C		
Maximum Temperature	Cleaning: 85°C		
Allowable nU	Continuous Operation: 3-9		
Allowable pH	Chemical Cleaning: 2-10.5		
<b>Maximum Pressure Drop</b>	<15psi		
Chlorine Tolerance	500ppm/h,dechlor is recommended		
Maximum Feed Turbidity	<1NTU		
Maximum Feed SDI (15 minutes)	<5		

### **Nominal Dimensions**



型号		尺寸-(in/mm)		
	A	В	C	
Dairy NF2-3838-31-C-0830	38 (965)	3.8 (97)	0.83 (21)	
DairyNF2 -3840-31/46-C-0830	38.75 (984)	3.8 (97)	0.83 (21)	
Dairy NF2-8038-31/46-C-1139	38 (965)	7.9 (200)	1.125 (28.6)	
DairyNF2-8040-31-C-1125	40 (1016)	7.9 (200)	1.125 (28.6)	

#### Important information

- New spiral membranes must be cleaned prior to first use. The cleaning procedure should be in accordance with the instructions provided in the HMCT cleaning description for the spiral membrane concerned.
- The customer is fully responsible for the effects that any incompatible chemicals may have on the spiral membranes.
- After initial wetting, the spiral membranes must be kept moist at all times.
- If the operating specifications provided in this product description are not strictly followed, the limited warranty will be null and void.
- To prevent biological growth during system shutdowns, HMCT recommends that spiral membranes should be immersed in a protective solution.
- Avoid permeate-side back pressure at all times.
- HMCT recommends using a rigid stainless steel ATD end device at the housing outlet end.
- HMCT recommends that the inner diameter of the housing should be approx. 2 mm (0.08") bigger than the outer diameter of the spiral membrane.
- For storage conditions, please see Storage document.
- For warranties, please see spiral membrane warranty document.

#### **Operating guidelines**

HMCT recommends the following start-up procedure from standstill to operating condition:

- The unpressurized plant should be refilled with water.
- Feed pressure should be gradually increased over a 30 60 second time scale.
- Before initiating cross-flow at high permeate flux condition (start-up with high-temperature water) the set feed pressure should be maintained for 5 10 minutes.
- Cross-flow velocity at the set operating point should be gradually achieved over a period of 15
   20 seconds.
- Temperature variations should be implemented gradually over a period of 3 5 minutes.
- Avoid any abrupt pressure or cross-flow variations on the membranes during start-up, shutdown, cleaning or other sequences in order to prevent possible damage.

